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Figure 4.7: Top: SEM image taken on the top surface of RAW004 inlet disk after SC CO₂ entry pressure measurements. Bottom: elemental mapping on the above image for Na and Cl.



Figure 4.8: Elemental mapping on the SEM image in Figure 4.7 for other major elements.



Figure 4.9: SEM image taken on the top surface of RAW004 middle disk after SC CO₂ entry pressure measurements.

Floment	Atom	Mass	Error
Element	at.%	wt.%	wt.%
Carbon ('C)	18.34	11.66	5.5
Oxygen (O)	56.31	47.69	18.9
Sodium (Na)	0.72	0.87	0.1
Magnesium (Mg)	1.07	1.38	0.1
Aluminum (Al)	7.96	11.38	0.7
Silicon (Si)	11.73	17.44	1.0
Phosphorus (P)	0.14	0.24	0.0
Sulfur (S)	0.06	0.11	0.0
Chlorine (Cl)	0.09	0.17	0.0
Potassium (K)	1.58	3.27	0.2
Titanium (Ti)	0.24	0.61	0.0
Iron (Fe)	1.75	5.18	0.2

Table 4.2:Elemental Analysis on the Image in Figure 4.9



Figure 4.10: Elemental mapping on the SEM images in Figure 4.9 for major elements.



Figure 4.11: SEM image taken on the bottom surface of RAW004 middle disk after SC CO₂ entry pressure measurements.



Figure 4.12: Elemental mapping on the SEM images in Figure 4.11 for major elements.



Figure 4.13: Top: SEM image taken on the top surface of RAW004 outlet disk after SC CO₂ entry pressure measurements. Bottom: elemental mapping on the above image for Na and Cl.



Figure 4.14: Elemental mapping on the SEM images in Figure 4.13 for other major elements.



Figure 4.15: A conceptual model of CO₂-brine interaction during CO₂ injection.

From the above image study, halite crystals were found along the edges of cracks close to the inlet of RAW004 after the SC CO₂ entry pressure measurement. The portion of core sample away from the inlet appeared to be similar to that before the CO₂ entry pressure test in both image and elemental analysis; no halite was observed. The halite crystals were probably due to the SC CO₂brine-rock interaction that is conceptually demonstrated in Figure 4.15. As dry SC CO₂ enters the rock, there can be two flows in opposite directions. At the upstream, dry SC CO₂ displaces the brine and vaporizes water in the brine. The evaporation concentrates the brine and leads to salt precipitation. Water is carried by CO_2 and moves downstream in the vapor phase. The evaporation can reduce the local water saturation below the equilibrium saturation for the applied capillary pressure (CO₂ injection pressure minus local water phase pressure). Water can consequently reimbibe towards the inlet, ie. water moves upstream in the liquid phase. As CO_2 pressure drops, water may also recondenses from the CO_2 near the outlet and dilutes the brine. This evaporation/condensation/imbibition cycle can transport additional salt towards the inlet. Therefore, halite precipitation should happen close to the inlet side. The dry-out and salt precipitation have been studied through coreflood experiments and numerical modeling [10] [11] [12] [13] [14].

Disk	Illite	Kaolinite	Chlorite-Fe	Calcite	Pyrite	K-Feldspar	Quartz
Inlet	27 (8)	24 (7)	5 (2)	6 (1)	3 (2)	6 (2)	29 (4)
Middle	20 (7)	22 (7)	5 (2)	10 (2)	4 (2)	7 (2)	32 (4)
Outlet	30 (9)	25 (8)	3 (2)	2 (1)	4 (2)	10 (3)	27 (4)

 Table 4.3:
 X-ray Diffraction Bulk Analysis on RAW004 after Entry Pressure Test

Results from XRD analysis on those three disks are summarized in Table 4.3 and Table 4.4, where the numbers in parentheses represent the estimated standard deviations at the 95% confidence level in unit of weight percent. Also note that the Clay Isolate Fraction analysis only covered those clay minerals with particle sizes from 0.26 to 4.7 microns. Both bulk and clay analysis suggested that the three disks from RAW004 had similar mineral compositions within the uncertainty range except for calcite. From Table 4.3, calcite was about 6 wt% in the inlet disk, 10 wt% in the middle disk, and 2 wt% in the outlet disk, respectively. The variation among disks appeared to be bigger than estimated

uncertainties. In comparison, no calcite was identified on the end-trim of RAW004 before the entry pressure test.

Disk	Illite	Kaolinite	Chlorite - Fe
Inlet	45 (14)	51 (14)	3 (3)
Middle	48 (14)	49 (14)	3 (3)
Outlet	45 (14)	51 (14)	4 (3)

Table 4.4:	X-ray Diffraction Analysis on Clay Isolate Fraction Components on RAW004 after
	Entry Pressure Test

Precipitation of calcite highlighted the potential cation exchange followed by another SC CO₂-brine-rock interaction in pore space as listed below:

$$CO_2 + H_2O = H_2CO_3 = H^+ + HCO_3^-$$
 (4.1)

$$CaCO_3 + H_2CO_3 = Ca^{2+} + 2HCO_3^{-}.$$
 (4.2)

Moreover, it also suggested that the dominant process for CO_2 invading into RAW004 was diffusion instead of viscous flow. Generally the calcite dissolution/precipitation strongly depends on the pH value of the environment, which is in turn strongly impacted by the CO_2 partial pressure. If viscous flow occurred in the pore space, as SC CO_2 was continuously injected into the pore space, the formation brine would have been strongly acidified with pH as low as 5 [3]. Calcite precipitation would be much less possible in such an acid solution.

From the above XRD analysis, an order-of-magnitude estimation can be made on the effective CO₂ diffusion coefficient in the cap rock. Total precipitated calcite was estimated to be about 1 g or 0.01 mol, where weight of the three disks from RAW004 was estimated from the bulk volume and an approximate bulk density of 2.7 g/cc. Reactions in Eq. (4.1) and (4.2) showed that 2 mole of CO₂ is needed to generate 1 mole of calcite. The average CO₂ flux during the 673-hour measurement was about 6.5×10^{-6} mol/(cm² hr). On the other hand, formation brine in the inlet face of RAW004 was assumed to be fully saturated with CO₂ as it was in direct contact with SC CO₂ during the test. Under the measurement conditions, solubility of CO₂ was about 61.3 scf/stb or 10.8 cc/cc. So the molar concentration of CO₂ was 4.6×10^{-4} mol/cm³. At the outlet side, the amount of calcite was very low according to the XRD result, which suggested that the CO₂ diffusion front had not reached the outlet yet. CO₂ concentration should be close to the original value and was much lower compared to that at the inlet. The concentration gradient of CO₂ across the core plug with its outlet concentration ignored was about 3.4×10^{-4} mol/cm⁴. If its porosity was assumed to be 2%, an effective diffusion coefficient for CO₂ in RAW004 was estimated to be 3×10^{-4} cm²/s.

Note that calcium was not observed in the EDS spectrum on samples from those disks. This was possibly due to the process of Ar milling for sample preparation. One crushed sample after XRD was analyzed by EDS again and calcium was clearly identified. More study may be required to assess this issue.

5. Conclusion and Recommendation on Future Study

In conclusion, capillary entry pressure measurements on Quest MCS core plugs suggested no CO_2 entry for capillary pressure less than 999 psi. At the capillary pressure higher than 999 psi, the measured flow rate was independent of the pressure drop. It indicated that the cap rock was extremely tight such that the fluid transport was not viscous flow, nor can it be described by Darcy's Law. Instead, the fluid transport was dominated by the diffusion process and the CO_2 -brine-rock interaction.

SEM images obtained on the core sample RAW004 before and after SC CO₂ entry pressure measurement confirmed very tight pores with poor connectivity in the cap rock. Those images also revealed halite crystals along the edges of micro-cracks close to the inlet side, which were not observed on sample before the CO₂ test. XRD analysis showed the presence of calcite after the CO₂ test. The elemental study provided strong evidence on the SC CO₂-brine-rock interaction, including evaporation, dry-out, precipitation, and brine imbibition. More importantly, the presence of calcite and the variation in its amount along the core plug strongly suggested that diffusion was the dominant process for mass transfer inside the pore space. Precipitation of calcite reduces the CO₂ concentration, and may also serve as a barrier to the CO₂ diffusive flow.

The caprock study in this work demonstrated that there are strongly coupled physical and chemical processes between SC CO_2 and water saturated rock. Therefore integration of different measurements, analysis, and numerical modeling is a must for future cap rock integrity assessment. The following types of tests/analysis are strongly recommended: capillary entry pressure measurement, mineralogy, imaging and elemental analysis before and after entry pressure test, and composition analysis on water before and after entry pressure test.

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Appendix 1.

This Appendix captures the capillary entry pressure measurements on a tight gas plug in 2008. It served as a basis to establish the measurement protocol. The setup consisted of a pressure confining core holder, a diaphragm, three displacement pumps, pressure transducers, and valves. All three pumps could inject or withdraw fluid at constant rate or under constant pressure. Note that for those displacement type pumps used in this work, volume changes were recorded in the opposite direction to that shown in Figure 2.1. Any production at the downstream side was indicated by the volume decrease in the back pump. A 10 cc diaphragm was used to separate CO_2 from the working fluid (Soltrol) of the injection pump. The whole setup was enclosed in a temperature controlled box and maintained at 50 °C during the test. A tight gas core plug sample was used to mimic the caprock. It had a porosity of 5% and permeability of 0.003 mD. The effective stress on the plug was 800 psi, and the back pressure was maintained at 1280 psi.



Figure A1.1: Delta pressure and pump volume changes during the SC CO₂ entry pressure measurement on a tight gas core plug (top chart), with the portion highlighted by dashed circle magnified in the bottom chart to show the CO₂ entry (indicated by arrows).

The capillary entry pressure was measured by a step-wise steady-state method as outlined below:

- The system was leak tested using a dry Berea core plug filled with dry SC CO₂ at about 1250 1300 psi and 800 psi effective stress for 7 days.
- The sample was vacuumed over 12 hours and saturated with 7% de-gased brine (the "dead brine"). The dead brine in the core plug was then displaced by "live brine" (7% brine saturated with CO₂ at 1215 psi and 50 °C) at a rate of 1 cc/day for about 5 pore volumes.
- After the live brine injection was finished and the back pressure was stabilized, dry SC CO₂ was injected at a rate of 1 cc/day while the back pressure was maintained at 1280 psi. The effective stress (confining pressure minus the injection pressure) was 800 psi.
- SC CO₂ was injected continuously until the preset pressure drop ($\Delta P = P_i P_b$) across the sample was reached. Then the injection pump was switched to maintain that pressure drop automatically for 6 hours or longer.
- At each preset pressure drop, the volume change of the back pump was monitored and recorded. Entry pressure was determined from the back pump movement.



Figure A1.2: Flow rate at each delta pressure during the SC CO₂ entry pressure measurement on a tight gas core plug.

Figure A1.1 shows the pressure drop (ΔP) across the core plug, as well as volume changes in injection and back pumps during the measurement. Where ΔP was set at 4.5, 8.9, 19.8, 25.9, 35.5, 76.5, 95.2, and 105.2 psi, respectively. During the first 39 hours of the injection, SC CO₂ was displacing the brine in the upstream tubing and end-piece. The back pump moved slightly to accommodate the brine production. When the CO₂ front reached the top surface of the core plug at $t_{exp} \approx 39$ hr, $\Delta P = 19.8$ psi, the CO₂ pressure was lower than the capillary entry pressure. Therefore, no more brine was displaced and the back pump volume stopped changing. After that the CO₂ pressure was increased in steps. When $\Delta P < 53$ psi, no brine was produced and the back pump did not move. Fluctuations in the measured pressure were due to the unoptimized pump control parameters. The back pump started moving at $\Delta P = 53$ psi or $t_{exp} \approx 127$ hr, which indicated capillary entry. When $t_{exp} > 148$ hr and $\Delta P = 95.2$ psi, CO₂ flow path was fully established in the core plug.

The back pump started moving at the same rate as that of the injection pump. The movement in both pumps increased proportionally as the pressure drop increased to 105.2 psi ($t_{exp} > 200$ hr). The measured flow rate verses the pressure drop across the sample is plotted in Figure A1.2, where the flow rate was calculated from the back pump volume change. Figure A1.2 is the relation between pressure drop and the flow rate. It shows that after the CO₂ breakthough the flow rate was proportional to the pressure drop as described by Dary's Law.

After the above entry pressure experiment, a stressed mercury capillary pressure curve was measured on the same core plug. The measured mercury entry pressure was 775.6 psi. From interface tension (32 dyne/cm) and contact angle ($\theta = 45^{\circ}$) of SC CO₂ [4] [15], the corresponding SC CO₂ entry pressure calculated from the mercury entry pressure was 48 psi, which agreed reasonably with the measured value (53 psi).

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