Using denitrifying bioreactors as a beneficial management practice for agricultural drainage waters in Alberta

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Executive Summary

In Alberta, sub-surface drainage is a common agricultural w ater management practice that removes excess w ater from the soil profile to improve soil moisture conditions for seeding and crop grow th. How ever, sub-surface drainage systems provide direct conduits for transporting nutrients from agricultural fields to surrounding w ater bodies such as irrigation canals, reservoirs and streams. Elevated concentrations of dissolved nutrients, such as nitrogen (N) and phosphorus (P), in drainage w ater can lead to w ater quality impairments including eutrophication of rivers and lakes, toxic algal blooms and potential damage to, and delayed w ater conveyance in, irrigation infrastructure due to buildup of w eeds and algae. Simple, low cost technologies are needed to reduce nutrient export from agricultural sub-surface drainage to sensitive aquatic ecosystems. A potential solution is the use of denitrifying bioreactors– a passive treatment approach w here drainage w ater is routed through solid carbon substrates to remove dissolved nutrients through physicochemical and biological processes. This edge-of-field w ater treatment technology is gaining popularity in the mid-w estern United States and eastern Canada, but has not gained w idespread acceptance in the Canadian Prairies. Consequently, there remains uncertainty as to w hether these technologies are appropriate for the Canadian Prairies considering agricultural drainage is greatest during spring snow melt and the bioreactor s are driven by biological processes, w hich may be inhibited by cooler spring temperatures.

This study evaluated the performance of pilot-scale denitrifying bioreactors for removing dissolved nutrients under Alberta agricultural field conditions at tw o representative geographic locations. Substrates w ere sourced from local materials and included w ood chips, hemp straw and barley straw . The substrates w ere tested under varying hydraulic retention times (flow rates) and temperatures from the beginning of the grow ing season in the spring to the end of irrigation season in fall for nutrient removal potential. Results from this study identified temperature, flow rate, carbon source material and bioreactor age as primary factors affecting nitrate removal. The flow design demonstrated that the low est flow rate maximized nitrate removal efficiency and w as further optimized in the w armer summer season. There appears to be a possible decline of nitrate removal capacity over time.

Overall, the average nitrate-N load reduction as a percentage of inlet load for the various treatments w as 45%, 59% and 36% for spring, summer and fall, respectively. The load reductions w ere significantly low er for the w ood chips (32%) compared to the agricultural residues (hemp at 50%, barley at 58%). Denitrifying bioreactor performance appears to be improved w ith the use of agricultural residues (barley straw and hemp straw) as fill media as compared to w ood, although the retention time als o influenced the overall nitrate removal capacity.

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1 Introduction

In Alberta, sub-surface drainage is an agricultural w ater management practice that facilitates crop grow th improvements by reducing excess soil w ater in the rooting zone. This practice is gaining popularity in Alberta's agricultural sector in response to increasing land values and a desire to maximize yield and achieve product consistency under variable topography, soil texture and precipitation patterns. This practice can also increase the soil absorption capacity betw een rain events and reduce overland sediment and contaminant transport in areas prone to surface runoff. By managing soil saturation, sub-surface drainage can result in a net reduction of non-point source pollution to receiving w ater bodies occurring through surface runoff. How ever, this results in sub-surface transport of soluble nutrients w ith a point source discharge at a central outlet. The accumulation of nutrients discharged from several outlets can have w ide-ranging consequences to receiving w ater bodies including rivers, reservoirs, irrigation canals and return flow channels.

Recent research and development efforts in the Midw estern United States have demonstrated the applicability of denitrifying bioreactors as an end-of-pipe treatment method for mitigating impacts from agricultural drainage w aters. How ever, unlike the Midw estern United States, the highest drainage rates in Alberta generally occur during snow melt in early spring under cool temperature periods in w hich biological activity may be substantively reduced. Consequently, uncertainty exists in applying denitrifying bioreactors to Alberta's agricultural landscape as design parameters have not been tested or optimized for the Canadian Prairies. This project evaluated bioreactor performance based on Alberta climate conditions and w ill allow stakeholders such as farmers, irrigation districts and regulators to assess the suitability of these systems w ithin their local context.

2 Objectives

The goal of this study w as to evaluate the feasibility and optimize the design criteria of denitrifying bioreactors as an edge-offield beneficial management practice (BMP) for mitigating environmental effects of agricultural drainage in Alberta. Project objectives outline the need for comparisons to be made betw een bioreactor performance in different geographic locations and w ith different design parameters to better understand such influences on bioreactor nutrient removal in Alberta.

Objective 1: Construct nine replicated pilot-scale bioreactors at each of the central (Edmonton) and southern (Taber) Alberta locations.

To account for interprovincial climatic variation, nine pilot-scale bioreactors w ere installed at each of tw o sites: one set w as located in central Alberta at the Crop Diversification Centre North (CDCN) and one set w as located in southern Alberta w ithin the Taber Irrigation District (TID). These locations represent different climate conditions common to Alberta's primary agricultural region and, as such, differ in their relative temperatures, precipitation patterns, day lengths, grow ing degree days, grow ing season lengths and soil types. These climates w ere humid continental in central Alberta and semi-arid in the south. At the CDCN site, the soil w as a Black Chernozem and at the TID site, the soil w as a Brow n Chernozem.

Objective 2: Assess the efficacy of local carbon feedstocks for reducing annual nutrient loading under climatic conditions common to Alberta.

Much of the field-based research completed on denitrifying bioreactors focuses on the use of w ood chips as a carbon-based feedstock to stimulate biological denitrification (Dougherty, 2018). Wood-based substrates are recommended for their physical durability, but laboratory studies have show n that denitrification rates in w ood-based bioreactors are hampered under cold temperatures due to low er emission of labile carbon (Cameron and Schipper, 2010). Agricultural residues such as straw , have demonstrated greater success at stimulating denitrification in cold temperatures (Feyereisen et al., 2016), but have not been subject to field-performance testing to any significant

degree that could inform their suitability as a bioreactor feedstock in Alberta. In this study, hemp straw and barley straw w ere compared w ith w ood chips as a bioreactor feedstock at each site.

Objective 3: Evaluate the effect of hydraulic retention time on nutrient load reductions by changing the retention times from the beginning of the spring to the end of the fall.

Cool temperatures reduce the rate of biological processes, such as denitrification, increasing the time required to achieve equivalent levels of biological activity under w armer temperatures. Much of the literature on field applications for denitrifying bioreactors describe studies that have been completed in w armer climates w here agricultural drainage is primarily driven through grow ing-season rainfall events (Feyereisen et al., 2016). As a result, the recommended hydraulic retention times reported in the literature may be unsuitable for conditions in Alberta, w here agricultural drainage is primarily snow melt-driven and occurs in the spring w hen temperatures are cool. Hydraulic retention times (HRT) of 4, 8 and 12 hours w ere compared at both sites to evaluate the relative effectiveness of increasing retention time on nutrient removal.

3 Methodology

3.1 Site Selection

Tw o sites that represent different climatic areas of Alberta w ere selected to install replicated pilot-scale bioreactors. The CDCN site w as located just outside of Edmonton and represented a humid continental climate (Figure 1) and the TID site w as located just outside of Taber and represented a semi-arid climate (Figure 2). Alberta's primary agriculture region spans both these climates.

3.2 Bioreactor Design and Construction

Nine replicated pilot-scale bioreactors w ere installed at each site in the fall of 2019. A trench-style bioreactor design w as used, as it represents a simple and practical w ay for producers to use bioreactor technology to intercept and treat subsurface drainage w ater. Each trench w as excavated to approximate dimensions of 6 m length \times 0.6 m w idth \times 1.3 m depth. Prefabricated liners (30 mil Linear Low Density Polyethylene) w ere then fixed w ithin the trenches to cover the bottom and sides, w ith extra to fold over the top after filling. The trenches w ere filled w ith one of three types of carbon-rich organic substrates. Wood chips, hemp straw and barley straw w ere used at both sites; the w ood chips (a by-product of pow er pole manufacturing) w ere obtained from a common source and hemp straw and barley straw w ere procured from a local producer proximal to each site. Each bioreactor w as filled w ith organic substrate. The hemp and barley straw came in the form of large square bales; staff cut the tying strings and then broke off slices from the bale. Slices w ere then placed in the trench and around the test pipes/w ells. Each layer of straw w as packed dow n as tightly as possible and the trench w as filled until it reached beyond the top of the bioreactor. The w ood chips w ere in a loose form, so w ere shoveled into the trenches, and then packed dow n as tightly as possible. Once trenches w ere full of either straw or w ood chips, the plastic liner w as then folded over the top of the material and covered w ith soil. Inflow and outflow pipes w ere placed at either ends of the bioreactors. Four w ells made of 10.2 cm (4 in.) polyvinyl chloride (PVC) tubing w ere installed at the start and end positions of the bioreactors and at tw o middle positions located at 1.8 m and 3.6 m from the first w ell. Water levels and w ater temperature w ithin the bioreactors w ere continually monitored throughout the study using pressure transducers to calculate the depth of the saturated zone (Figure 3). The w ells allow ed for collection of w ater samples from w ithin the bioreactor. The inlet w ater w as fed from the top of the inlet w ell, and the outlet port w as positioned to maintain a saturated depth of approximately 1 m w ithin the bioreactors (Figure 4).

Figure 1. (a) Bioreactors at CDCN (b) CDCN Bioreactor identification and feedstock schematic.

Figure 2. (a) Bioreactors at TID (b) TID Bioreactor identification and feedstock schematic

Figure 3. Sampling well with pressure transducer removed and resting on cap awaiting download.

Figure 4. Dimensional schematic of pilot-scale bioreactors in longitudinal cross-section.

Water w as diverted from an adjacent stream for the CDCN site and from an irrigation canal at the TID site to supply w ater to the bioreactors. Water w as pumped from the stream or canal, filtered to <100 µm using an automated self-cleaning filter and dosed to approximately 20 mg/L of nitrate using a dosing pump attached to a large stock tank. Stock solutions of nitrate w ere prepared w eekly using filtered stream/canal w ater and potassium nitrate fertilizer. Flow into each bioreactor w as controlled w ith valves and flow meters attached to each inlet pump. Flow control w as required to achieve the desired (theoretical) HRT in order to compare the effect of different HRTs on nutrient removal performance.

3.3 Physical and Hydraulic Properties

Tracer tests w ere conducted in order to characterize each bioreactor in terms of physical and hydraulic properties. One kilogram of sodium chloride (NaCl) (4 L of 250 mg/L solution) w as added to each bioreactor and the change in specific conductance (SpC) w as monitored at the outlet w ell using deployable conductivity sensors capable of continuous monitoring. Calibration curves w ere established from each event to calculate solute mass transport from conductivity measurements. These measurements enabled the calculation of the actual hydraulic retention time as w ell as additional hydraulic properties for each substrate under different flow conditions, such as hydraulic efficiency, solute dispersion– using the Morrill Dispersion Index (MDI) and preferential flow – using the short-circuiting index (S). These hydraulic properties w ere used to determine the flow rates needed to achieve the various retention times for each type of feedstock bioreactor.

Hydraulic efficiency w as calculated as the ratio of mean solute retention time to the time of peak concentration (Persson et al., 1999) and it indicates the departure of the average retention time of solutes from the target HRT. Hydraulic efficiency values fall w ithin 0.0 – 1.0, w ith 1.0 being the most ideal as it represents unimpeded flow or greatest hydraulic efficiency. How ever, values above 0.5 indicate conditions that allow for effective flow and are considered satisfactory for a w orking bioreactor. The MDI is an indicator of dispersion and mixing of the tracer throughout the bioreactor, w here low er values (i.e. near zero) indicate less mixing and less contact w ith the feedstock material and MDI values from 1.0- 2.0 indicate plugged flow , or more opportunity for mixing. A high MDI indicates the tracer w as w idely distributed throughout the bioreactor and the resulting tracer curve typically show s a w ide peak rather than a sharp one (Dougherty, 2018). The short-circuiting index (S) indicates the degree of preferential flow paths occurring in the bioreactors; an S value of 1.0 indicates uniform flow across the bioreactor, w hich is most effective for nitrate removal. S values less than 1.0 indicate that preferential flow or short-circuiting is occurring, w hich means the w ater quickly flow s through the feedstock w ith little opportunity for nitrate removal (Hoover et al., 2017).

Saturated hydraulic conductivity (Ksat) w as calculated using a slug test in w hich a 9 cm diameter bailer (~5 L volume) w as low ered into one of the internal w ells in the bioreactor to remove a volume or 'slug' of w ater. The recovery of the w ater lev el w as measured using a pressure transducer set to record w ater levels every 0.5 seconds to account for the rapid recovery of the w ater level in the substrates. The slug tests w ere performed at each site at the end of each season.

3.4 Experimental Design

3.4.1 2020 Field Season (CDCN and TID)

In 2020, the study w as designed in a w ay that at each site (CDCN and TID) and each feedstock material (three bioreactors each of w ood, hemp and barley) w ould be combined w ith each HRT treatment (4, 8 and 12 h), to test the interactive effect betw een the treatments. As a result, these target HRTs w ere cycled betw een seasons throughout 2020 and the tracer tests w ere conducted at the start and end of the seasonal assessment. The flow rates in each bioreactor w ere adjusted to a different HRT level in each seasonal assessment (spring, summer and fall). Slug tests w ere also performed in order to characterize the physical stability of the feedstocks.

3.4.2 2021 Field Season (TID)

In 2021, Government of Alberta (GOA) staff w ere unable to operate the bioreactors at CDCN and each bioreactor at TID w as run through the same flow -recession design each season, w hich allow ed for a direct comparison of treatment performance betw een feedstocks during each assessment period. This flow -recession design mimicked natural conditions of high- to low flow conditions during a runoff event. The bioreactors started at a flow rate of 2 GPM (US gallons per minute) (~5 h HRT), follow ed by successive declines to 1.5 GPM (~7.5 h HRT) and 1 GPM (~10 h) each season. The duration of each flow rate w as approximately one w eek. Three seasonal assessment periods w ere conducted (spring, summer and fall) to account for seasonal differences in treatment performance. Corresponding tracer studies w ere conducted at the start of each seasonal assessment at a flow rate of 2 GPM only w ith slug tests performed at the end.

3.5 Bioreactor Assessment

Assessment of bioreactor performance for removing dissolved nitrogen w as conducted on a seasonal basis throughout the grow ing period, focusing on spring (May–June), summer (July–August) and fall (September–October) seasons. During each seasonal assessment, nitrate-dosed w ater w as pumped through the bioreactors continuously for approximately four w eeks w ith a three- to four-w eek shutdow n period in betw een seasons during w hich no w ater flow ed in the bioreactors.

Bioreactor performance w as assessed using the difference in concentrations from the inlet to the outlet w ell positions. Cumulative nitrate-N mass loads entering and exiting the bioreactor w ere calculated by multiplying the incremental flow volume (measured at the inlet w ells using continuous loggers) by the nitrate concentration (from the inlet and outlet positions), and then summing those incremental loads over each monitoring period or season (spring, summer and fall), expressed as mass per unit of time. During each seasonal assessment, w eekly w ater samples w ere collected from the outlet w ell using a bailer. Source w ater samples from the stream (CDCN) and the canal (TID) w ere also collected and analyzed in order to provide background concentrations prior to mixing the source w ater w ith nitrate fertilizer. Sample bottles w ere triple rinsed w ith sample w ater, then filled w ith as little headspace as possible. Sample bottles w ere placed in coolers w ith ice packs and shipped to the laboratory. They w ere analyzed for pH, electric conductivity (EC), ammonium nitrogen (NH₄-N), nitrate nitrogen $(NO₃-N)$, nitrite nitrogen $(NO₂-N)$ and alkalinity content. Mass loading of $NO₃-N$ into and out of the bioreactors w as calculated using cumulative flow (measured at the inlet w ells using continuous loggers) and nitrate concentrations. The laboratory analysis for this project w as conducted at Government of Alberta laboratories in Lethbridge for the first year of operation (2020) and at the ALS laboratory in Calgary for the second year (2021).

3.6 Statistical Analyses

In this study, three feedstock treatments w ere repeated in triplicate, with three HRT treatments within the feedstocks and repetition of HRT treatments w ithin the bioreactors. Therefore, a crossover repeated measures design w as used to determine nutrient removal performance and to account for w ithin-bioreactor variability and potential carry-over betw een HRT treatments. The analysis w as performed using Microsoft® Excel® (2016) and RStudio (2020). Cumulative load reductions w ere also calculated in both trial years to assess the temporal resilience in load reductions after overw intering. The Mann-Whitney Rank Sum test (using SigmaPlot (2011); P <0.05) w as also carried out to compare the hydraulic proprieties at TID for both years of operation. Boxplots and scatterplots w ere created in RStudio to provide visual displays of the w ater parameter concentrations.

4 Results

4.1 Physical and Hydraulic Properties

4.1.1 2020 Field Season (CDCN and TID)

Tracer tests w ere run at different targeted (theoretical) HRTs (4, 8 and 12 h) prior to each of the three seasonal assessment periods (spring, summer and fall) to collect information on the hydraulic properties of each bioreactor. At CDCN, all the peaks occurred in less than 15 hours after the injection (time 0) w hile at TID, all the peaks occurred in less than 10 hours (Figure 5). Overall, the time required for the salt w ave to pass varied from one hour to over 15 hours. The change in specific conductanc e during the salt w ave passage depended on the mixing characteristics of the bioreactors, how the bioreactors w ere constructed, and how the feedstocks w ere packed. The type of feedstock did not appear to affect specific conductance because the bioreactors filled w ith the same feedstock show ed different curves (Figure 5).

The physical and hydraulic properties measured in the bioreactors through slug and tracer tests w ere hydraulic conductivity, hydraulic efficiency, dispersion and short-circuiting. These properties, according to the feedstock and HRT for the first year of operation, are presented in Figure 6.

Figure 6. Hydraulic properties of the bioreactors as measured by (a) saturated hydraulic conductivity (m/s), (b) hydraulic efficiency (unitless), (c) Morrill Dispersion Index (unitless) and (d) Short-circuiting index (unitless) in 2020. Results are differentiated by feedstock type (barley, hemp and wood), theoretical hydraulic retention time (4, 8 and 12 h) and sites (CDCN and TID).

For the first year of operation, clear differences can be observed betw een sites. Saturated hydraulic conductivity (Ksat) demonstrated a consistent trend betw een feedstock types at both sites, w here w ood and hemp straw demonstrated greater conductivity than barley straw . Similarly, Feyereisen (2018) found higher hydraulic conductivities for w ood chips than barley straw (0.048 and 0.028 m s-1, respectively). The Ksat values w ere substantially greater at the CDCN site for all feedstock types, perhaps due to differences in the w ay the feedstock material w as packed or the freeze-thaw event betw een the installation (fall 2019) and the operation (spring 2020). Other studies have documented w ood chip hydraulic conductivities ranging from 0.03 m s⁻¹ (Christianson et al., 2020) to 0.05 m s⁻¹ (Feyereisen et al., 2016).

The w ood bioreactors show ed greater hydraulic efficiency values than other feedstock types at both sites w ith hydraulic efficiency values being greater at the CDCN site for hemp and w ood than the TID site. How ever, all the values (except for hemp at TID for 12 h HRT) w ere greater than 0.5, w hich is considered satisfactory.

The MDI, or degree of dispersion or mixing, w ithin the bioreactors at CDCN appeared to be greater in the barley straw bioreactors. In fact, the MDI w as consistently low er in the hemp and w ood bioreactors, as indicated by low er hydraulic efficiency and greater MDI values for barley straw . Conversely, the degree of dispersion w as relatively consistent among the barley and w ood bioreactors at the TID site, but w as greater in the hemp straw bioreactors.

Advancing denitrifying bioreactors as a beneficial management practice for agricultural drainage waters in Alberta 8 When short-circuiting exists (S values less than 1.0), a portion of the flow exits the bioreactor sooner than expected. The CDCN site had more ideal flow (i.e., higher S values: less short-circuiting) w ith S values in the order of w ood>hemp>barley, w hereas at the TID site barley straw had less short-circuiting than either hemp or w ood, in the order of hemp=w ood>barley.

Collectively, these first year results indicate that the physical and hydraulic properties of the bioreactors seemed to be more influenced by site than by either feedstock or hydraulic retention time.

Comparatively, for bioreactors filled w ith w ood chips, Hoover et al. (2017) reported values around 2.8, 0.78 and 0.73 for MDI, hydraulic efficiency and short circuiting, respectively, w hile Schaefer et al. (2021) reported values of 3.3, 0.70 and 0.66 for the same parameters, respectively. Gosh et al. (2020) also found values of 5.8, 0.45 and 0.56 for MDI, hydraulic efficiency and short circuiting respectively.

4.1.2 2021 Field Season (TID)

For the second year of operation, the experiment could only be conducted at the TID site. The tracer tests w ere run at a fixed flow rate of 2 GPM (~5 h HRT). Like in 2020, all the peaks occurred w ithin 10 hours after the injection and the time required for the salt w ave to pass varied from one hour to over 10 hours (Figure 7). The presence of multiple peaks (BIO5, BIO 6 and BIO8) may mean that a short circuiting stream or preferential flow existed in the bioreactor, producing different flow channels from the inlet to the outlet (Wang et al., 2015).

Figure 7. Time series of specific conductance after tracer tests for nine pilot-scale denitrifying bioreactors at TID after the summer 2021 seasonal test. Results are differentiated by feedstock type.

Physical and hydraulic properties (hydraulic conductivity, hydraulic efficiency, dispersion and short-circuiting) are presented in Figure 8. Wood chips demonstrated greater Ksat than hemp and barley straw . The w ood and barley bioreactors show ed hydraulic efficiency values greater than 0.5, w hile the hemp bioreactor show ed low er values as in the first year of operation. The MDI w as relatively consistent among all the bioreactors at the TID site, but w as slightly greater in the hemp bioreactors. Like the first year of operation, barley straw show ed a low er degree of short-circuiting (low er S values) than either hemp straw or w ood chips at the TID site.

Figure 8. Hydraulic properties of the TID bioreactors as measured by (a) saturated hydraulic conductivity (m/s), (b) hydraulic efficiency (unitless), (c) Morrill Dispersion Index (unitless) and (d) Short-circuiting index (unitless) in 2021. Results were collected at 2 GPM (~5 h HRT) and are differentiated by feedstock type (barley, hemp, wood). Dots denote outliers.

4.1.3 Overall Assessment (TID)

After tw o years of operation, the hydraulic properties at TID w ere compared. Table 1 and Table 2 report the mean and median values, respectively.

TABLE 2. MEDIAN VALUES FOR THE ASSESSMENT PERIODS FOR 2020 AND 2021 ACCORDING TO THE FEEDSTOCK MATERIAL

There w as a statistically significant difference in the median Ksat values for hemp in 2020 compared to 2021 (Mann-Whitney Rank Sum Test, P < 0.05). This might explain the differences in performance of the bioreactors. There w ere no statistically significant differences betw een median values for the other feedstocks and parameters.

The range of the hydraulic efficiency remained the same for both years w ith no statistically significant difference betw een their median values.

The mean MDI values for 2020 (4.10 to 5.64) w ere greater than the 2021 MDI values for all bioreactors (3.79 to 5.01). This suggests a slightly greater flow dispersion in the first year of operation; how ever, there w ere no statistically significant differences in the median values betw een years. Calculated MDIs in this study are similar to other reported MDI values for w ood feedstock (Christianson et al., 2011).

Average short-circuiting values increased in all the bioreactors in 2021: the mean S values for 2020 (0.5 to 0.57) w ere low er than the mean 2021 S values for all bioreactors (0.52 to 0.65). This suggests that less short-circuiting occurred in 2021, w hich means potential for denitrification increased because the w ater flow ed through the bioreactor closer to the intended treatment time (Dougherty, 2018); how ever, there w ere no statistically significant differences in the median S values betw een years.

4.2 Nitrate Removal Performance of Bioreactors

4.2.1 2020 Field Season (CDCN and TID)

The capacity of bioreactors to remove nitrate under varying HRT conditions and feedstock materials w as assessed through w eekly sampling during the target seasons. The observed percentages of nitrate removal w ere determined as a function of the ratio of the concentration of nitrate at the inlet and outlet positions, compared against the total mass of nitrogen added during the assessment periods for 2020 (Figure 9). In general, the nitrate removal performance of bioreactors filled w ith agricultural residues (hemp and barley straw) tended to fluctuate around a mean value and did not exhibit positive or negative trends as nitrate w as cumulatively added to the systems in 2020. How ever, the w ood chips, particularly at 8 h and 12 h retention times, show ed increased nitrate removal performance as the cumulative mass of nitrate increased in the system. This may reflect a

difference in the capacity of the materials to harbour populations of denitrifying bacteria, or it may be a function of assimilatory nitrate uptake given the greater carbon-to-nitrogen ratio present in w oody biomass compared to agricultural residues. Thus, it appears that in the first year of operation, agricultural residues demonstrate a stable and relatively consistent capacity to remove nitrate. How ever, the retention time and material type have a clear influence on overall nitrate removal capacity.

Figure 9. Percentage of nitrate removal between inlet and outlets of bioreactors versus the cumulative mass of nitrate added (kg) according to the target hydraulic retention time (4, 8, or 12 h) and feedstock material for all the sampling dates in 2020.

As mentioned, nitrate removal performance w as defined as the percentage of nitrate mass removed as w ater flow ed from the inlet to outlet w ell positions. Substantive differences in overall nitrate removal performance betw een feedstock types w ere evident during the spring, summer and fall assessment periods, for both sites, in the 1,544 samples collected (Figure 10). The agricultural residues tended to exhibit greater denitrification, or nitrate removal, than w ood chips under all design HRTs. The

cooler temperatures during the fall assessment period seemingly decreased the denitrification rates observed in all bioreactors.

Figure 10. Overall percentage of nitrate removed during the spring, summer and fall assessment periods according to the theoretical hydraulic retention time (4, 8, or 12 h) and feedstock material for 2020 (TID and CDCN combined, N=1,544 samples).

Table 3 show s the mean values per assessment period and feedstock. Wood chips show ed the low est mean value during each season at the TID site and during spring and summer at the CDCN site. During the summer, barley straw show ed the greatest overall mean nitrate reduction for both sites.

At both sites, hemp straw show ed the greatest nitrate reduction in the spring then declined though the year (first year of operation). Barley straw show ed the greatest nitrate reduction in the summer. Wood chips varied betw een sites, show ing the greatest nitrate reduction in the spring at CDCN site and during the summer at the TID site.

TABLE 3. MEAN VALUES OF NITRATE REDUCTION (%) IN EACH ASSESSMENT PERIOD FOR 2020 AND FEEDSTOCK MATERIAL AT THE CDCN AND TID SITE

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Collectively, barley straw w as more effective (58%) than w ood chips (32%) for nutrient removal w hile hemp straw show ed a nitrate reduction of 50%. These findings w ere consistent w ith values reported in the literature. Several studies have documented nitrate reduction for w ood bioreactors, w hich w as commonly about 50% (Faramarzmanesh et al., 2021; Hassapour et al., 2017; Wrightw ood et al., 2022), although they range from 51 to 90% (Gosh et al., 2020), from 40 to 90% (Diaz-Garcia et al., 2021), from 46 to 68% (Christianson et al., 2020), from 8 to 55% as HRT increased (Hoover et al., 2016) and from 45 to 99% (Rivas et al., 2019).

Research conducted by Hashemi et al. (2010) show ed a nitrate reduction for laboratory denitrification bioreactors from 60.22 to 69.87% for barley straw w hile Kouanda (2021) reported a nitrate reduction of 15.25% for barley straw and 11.01% for w ood, Hellman et al. (2021) reported a nitrate reduction of 42% for barley and 44% for w ood.

At both sites, the source w ater (i.e. prior to mixing w ith fertilizer) had nitrate values below 10 mg L-1 and pH values w ithin the range know n to be ideal for denitrification ($pH = 7.5-9.5$) – outside this range, denitrification rates have been show n to decrease (Albina et al., 2019).

To provide a visualization of nitrate removal, measured nitrate concentrations in the inlet w ell of CDCN 1-1 (Inflow) and outlet w ell CDCN 1-4 (Outflow) from May through October 2020 from one of the w ood-filled bioreactors at the CDCN site (bioreactor 1) are show n in Figure 11. The closer the inlet concentrations are to the outlet concentrations, the less nitrogen is being removed. Through this period, inlet Nitrate-N averaged 24.9 mg L-1. Outlet nitrate-N concentrations w ere elevated in spring, coinciding w ith low temperatures and snow melt runoff; they decreased w ith increasing temperatures and increased at the beginning of fall.

4.2.2 2021 Field Season (TID)

As mentioned, in 2021, only the TID bioreactors w ere operational. All nine bioreactors operated on the same flow schedule, w hich allow ed for a direct comparison of treatment performance betw een feedstocks during the assessment period. As the total mass of nitrate injected into the system increased w ith time, the flow rate w as decreased to evaluate the effect of HRT on nitrate removal.

The observed percentages of nitrate removal, as a function of the ratio of the concentration of nitrate at the inlet and outlet positions, compared against the total mass of nitrogen added during the assessment periods for 2021 are presented in Figure 12.

Nitrate Removal percentage as function of the cumulative mass of nitrate added has the highest removal in summer, remaining almost constant during the fall. The bioreactors w ere run only tw o w eeks in the spring due technical problems , explaining the decreased mass added to the system during this time.

As in 2020, nitrate removal performance in 2021 w as determined by the percentage of nitrate mass removed as w ater flow ed from the inlet to outlet w ell positions. Substantive differences in overall nitrate removal performance among the feedstock types w as evident during the spring, summer and fall assessment periods (Figure 13). The bioreactors tended to exhibit greater denitrification under low er flow rates during the summer season. The w armer temperatures during the summer assessment period likely increased the denitrification rates in all bioreactors.

Figure 13. Overall percentage of nitrate removed during the spring, summer and fall assessment periods according to the flow rate (2 GPM, 1.5 GPM, or 1 GPM) and feedstock material for the TID site in 2021.

4.2.3 Overall Assessment

For the bioreactors at the TID site in the first year of operation, there w as a greater rate of nitrate removal w hile the overall performance during the second year decreased, especially for the spring and fall periods. Overall, barley show ed the best performance w hile w ood show ed the poorest (Figure 14).

Figure 14. Overall percentage of nitrate removed during the six assessment periods according to the feedstock material for CDCN and TID. CDCN only operated in 2020, while TID operated in 2020 and 2021.

After tw o years of operation at TID, the nitrate removal performance of all feedstocks combined in 2020 w ere compared to that of all feedstocks combined in 2021. It w as found that nitrate removal performance in 2021 w as significantly less than in 2020 (p= 0.002) according to results of a Mann-Whitney Rank Sum Test (Table 4). Wood chips show ed the low est mean nitrate reduction during each season.

With the exception of hemp straw in 2020, all other bioreactors at the TID site show ed peak performance during the summer seasons, indicating that temperatures w ere a crucial factor in the performance as highlighted by Hoover et al. (2016). Greatest year-on-year declines occurred in spring for all feedstocks. Barley straw saw the greatest overall reduction in the second year of operation.

Some studies have documented a decrease in nitrate reduction after the first year of operation. Rivas et al. (2019) reported a decrease from 99% to 48% for w ood bioreactors w ithin tw o years of operation w hile Gosh et al. (2020) reported a decrease from 90.2 to 51.0% from the first year to the second, but an increase to 84.9% in the third year of operation of w ood chip bioreactors.

TABLE 4. MEAN VALUES OF NITRATE REDUCTION (%) IN EACH ASSESSMENT PERIOD FOR 2020 AND 2021 AND FEEDSTOCK MATERIAL AT THE TID SITE

Nitrate concentrations in the inlet w ell TID 1-1 (Inflow) and outlet w ell TID 1-4 (Outflow) from May to Sept 2020 and May through October 2021 at the TID site are show n in Figure 15. The low est nitrogen concentrations observed in the outflow monitoring w ell indicate high rates of nitrate removal and occurred during all three seasons during the first year of operation and during the summer season of the second year.

Figure 15. Concentration of nitrate removed during the spring, summer and fall assessment periods for (a) 2020 and (b) 2021 at the inlet well (TID 1-1) and monitoring well (TID 1-4) at the first bioreactor (barley) at the TID site.

5 Conclusions

5.1 Physical and Hydraulic Properties

Based on the physical and hydraulic properties measured by slug and tracer tests at both sites, agricultural residues (barley straw and hemp straw) performed at varying degrees. Hydraulic conductivity and efficiency, as w ell as optimal mixing and consistent flow patterns throughout the bioreactors w ere achieved and sometimes optimized by agricultural residues. Nevertheless, there w ere notable differences betw een locations and time of year, demonstrating the impacts that temperature and moisture conditions are know n to have on denitrification. There w ere no consistent trends in properties among feedstocks or sites, w hich may indicate that the hydraulic properties of the bioreactors w ere more influenced by construction methods during bioreactor installation rather than the functional attributes of either feedstock material, hydraulic retention time or geographic location in the province. Construction methods that may affect physical or hydraulic properties of the bioreactors could be the method of packing or amount of feedstock used. One w ay to mitigate this could be to use a pre-measured volume for each bioreactor to ensure the same amount of measured feedstocks are used and that the same placement techniques are performed. It is recommended that slug and tracer tests be conducted upon installation of denitrifying bioreactors to ensure physical and hydraulic properties are conducive to effective operation.

5.2 Nitrate Removal Performance of Bioreactors

When compared to w ood chips, the amount of nitrate removed by agricultural residue w as consistent over the seasonal operation of the bioreactor (i.e., similar performance at beginning and end of month-long seasonal trials). In contrast, the removal of nitrate by the w ood chips w as maximized as the cumulative mass of nitrate increased w ith time. The differences in surface area or size of the feedstock pieces might have influenced the differences observed betw een the performance of w ood chips and agricultural residues in that the feedstocks act as a filter and the 'filter size' is defined by the size of the feedstock pieces. How ever further research on this possibility is needed.

Nitrate removal w as optimized by longer hydraulic retention times and w armer temperatures as evidenced by slow est flow rates and the highest nitrate removal during the w armer summer seasonal trials, respectively.

The nitrate reductions for the w ood chips and barley straw w ere consistent w ith w hat other researchers have found w ith the first year of operation show ing the greatest reduction.

Looking at performance over time, the bioreactors at the TID site show ed the greatest rates of nitrate removal during the first year of operation, w hile the overall performance during the second year decreased, especially f or the spring and fall periods. Overall, barley straw show ed the best performance w hile the w ood show ed the poorest. The barley straw performance w as optimized in summer, w hich suggests that w arm w eather played an important role. When comparing the tw o sites in 2020, the bioreactors at CDCN show ed greater mean values of nitrate reduction during almost all assessment periods and w ithin all feedstocks.

The observed results are promising given that agricultural residues are readily available in agricultural landscapes throughout Alberta. These results, how ever, only reflect one year of operation for the bioreactors located in central Alberta and tw o years for the bioreactors located in southern Alberta and so do not reflect the temporal stability and durability of agricultural residues under longer-term operation.

6 Summary and Recommendations

This project evaluated the performance of pilot-scale denitrifying bioreactors for removing dissolved nutrients under varying agricultural field and climatic conditions in Alberta. Tw o representative geographic locations w ere selected for the study (Objective 1). Local biomass materials (w ood chips, hemp straw and barley straw) w ere tested for nutrient removal potential under varying retention times and ambient temperatures throughout the grow ing season (Objective 2). After installation of bioreactors at the tw o sites in fall 2019, sodium chloride tracer tests w ere conducted on each replicated bioreactor to

determine physical characteristics and flow parameters (Objective 3). This information w as used to determine the flow rates needed to achieve the various retention times for each type of feedstock bioreactor.

The tracer test results indicated that the hydraulic properties of the bioreactors seemed to be more influenced by the degree of packing during bioreactor construction and subsequent settling rather than the functional attributes of either feedstock or hydraulic retention time.

In summary, this study identified temperatures, flow rate (hydraulic retention time), carbon source material and age of the bioreactor as the primary factors affecting nitrate removal. The flow -recession design demonstrated that the low est flow rate maximized the nitrate removal efficiency. How ever, it w as highly related to the season as nitrate removal w as greater in summer. In general, there appears to be a possible decline of nitrate removal capacity over time; how ever, the effective bioreactor lifespan is still unknow n.

The use of readily-available/locally-sourced agricultural residues instead of w ood chips provides an attractive option, at least in the short-term, and an incentive to further explore this technology. It appears that agricultural residues tended to exhibit greater denitrification than w ood chips under all design HRTs. This may be a function of physical properties (size of individual w ood chips relative to barley/hemp straw) or chemical properties.

This project is a valuable contribution to the development of bioreactor technologies for drainage w ater management in Alberta to help the agricultural industry minimize its impact on the environment and protect dow nstream w ater bodies. How ever, prior to implementing the know ledge acquired, additional research is necessary. Recommendations for future research are:

- 1) Implementation and testing on a larger scale and for an extended time period (> 2 yr) prior to making recommendations for commercialization. A comparison w ith other comparable edge-of-field technologies for drainage w ater management such as w etlands, buffer strips and sediment control are w arranted. There is also a need for testing these practices and verifying the performance in different ecoregions in Alberta.
- 2) Long-term effectiveness of different feedstocks. A longer-term study is necessary to make recommendations about how often the feedstock should be replaced. According to Lepine et al. (2018), only a bioreactor w ith fresh w ood chips (i.e., one-year w ood chip replacement schedule) is likely to demonstrate maximum removal rates due to ideal flow conditions and available labile carbon. They highlighted that w hile N removal rates w ill likely be inconsistent from year to year; they show a general trend of decreased performance after one year of operation, though years tw o and onw ard tend to be similar.
- 3) Tests for mixing w ood chips w ith agricultural residues. Expecting better performance from mixing substrates is speculative, but it could be assumed that mixing a good performing substrate w ith a poorer performing substrate w ould result in a performance somew here in the middle.

The agricultural industry, as w ell as drainage contractors, have demonstrated interest in assisting w ith field-scale bioreactor installations, project coordination and communication of learnings.

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